

IN THE SPECIFICATION:

Page 4, please rewrite the paragraph at lines 2-18 as follows:

To solve the foregoing problems in conventional techniques, the inventors of the present invention assiduously studied about the conditions under which precipitated calcium carbonate was manufactured by blowing carbon dioxide containing gas into a calcium hydroxide slurry. As a result, they found that a calcium carbonate aggregate containing uniformly flocculated primary particles having a long diameter of 0.5 to 3.0 μm , a short diameter of 0.1 to 1.0 μm and an aspect ratio of ~~lower than 3 or more~~ can be obtained by using a high concentration calcium hydroxide slurry as raw material, and allowing a carbonation reaction to proceed in two stages under predetermined conditions, and that a calcium carbonate aggregate containing particles having such a shape exhibits extremely favorable dispersibility in pulp fiber and is effective for improving the bulk of paper, and thus accomplished the present invention.

Page 4, please rewrite the paragraph at lines 19-26 as follows:

That is, the precipitated calcium carbonate of the present invention is precipitated calcium carbonate having a diameter of 1 to 10 μm consisting of flocculated primary particles having a long diameter of 0.5 to 3.0 μm , a short diameter of 0.1 to 1.0 μm and an aspect ratio of ~~less than 3 or more~~, wherein the BET specific surface area is in the range of 8 to 20 m^2/g , and the pore volume is in the range of 1.5 to 3.5 cm^3/g .

Page 8, please rewrite the paragraph at lines 23-29 as follows:

The calcium carbonate obtained by the producing method of the present invention is flocculent aggregates having a secondary particle diameter of 1 to 10 μm and consisting of primary particles having a long diameter of 0.5 to 3.0 μm , a short diameter of 0.1 to 1.0 μm and an aspect ratio of ~~less than 3~~ or more. These flocculent aggregates have a large surface area and a large pore volume.

Page 12, please rewrite the paragraph at line 21 to page 9, line 8 as follows:

Carbonation reactions at the first stage were performed in the same manner as in Example 1, and, when the carbonation rates became 45%, 91% and 100%, the supply of the carbon dioxide containing gas was discontinued to terminate the reaction. The reaction mixture was added with 10% by weight of a calcium hydroxide slurry having a calcium hydroxide concentration of 100 g/L based on the amount of the reaction mixture, and a reaction at the second stage was performed at reaction start temperature of 61°C with further blowing in carbon dioxide containing gas. After the reaction, dehydration and classification were performed to obtain calcium carbonate. The shape of this calcium carbonate was observed by using an electron microscope, a laser particle size analyzer and an X-ray power diffractometer.